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川渝裂缝性地层自动压井环空 多相压力波速特性研究*

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摘要: 考虑虚拟质量力、环空沿程压力、气液相间阻力、气体滑脱、环空空隙率等因素, 基于小扰动理论, 提出了裂缝性地层自动压井环空多相压力波速数学模型, 结合半显式差分方法, 以彭州 PZ-5-3D 井 (垂深 5 827 m) 为实例, 对模型编程求解. 结果表明: 裂缝性地层出气具有段塞流特点, 随空隙率增大, 压力波速呈现先减小后增大趋势; 空隙率在 0% 至 16% 区间, 压力波速以液弹为主, 压力波速呈急剧下降趋势; 空隙率在 16% 至 40% 区间, 压力波速趋于平缓恒定值; 空隙率在 42% 至 100% 区间, 压力波速呈现增大趋势, 压力波速以气弹为主; 随环空井深减小, 环空空隙率减小, 压力波速整体呈现减小趋势; 随压井循环排气井口回压增大, 压力波速整体呈现增大趋势; 环空空隙率在 0% 至 13% 区间内, 气体滑脱速度对压力波速影响不大; 环空空隙率在 13% 至 85% 区间内, 随气体滑脱速度增大, 压力波速呈现减小趋势; 节流阀调阀时间间隔与井底压力响应时间具有跟随性, 随井底压力响应时间增大, 调阀时间间隔增大.

关键词: 裂缝性气藏; 自动压井; 环空多相流; 压力波速; 气体滑脱

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Study on Multiphase Pressure Wave Velocity Characteristics of Automatic Kill Annulus in Chuanyu Fractured Formation

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Abstract: In view of the virtual mass force, the annulus pressure, the gas-liquid resistance, the gas slippage, the annulus void fraction and other factors, the mathematical model for annular multiphase pressure wave velocities of automatic kill in fractured formation, was proposed based on the small perturbation theory. With the Pengzhou PZ-5-3D well (vertical depth

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5 827 m) as an example, the model was solved programmatically with the semi-explicit difference method. The results show that, the gas from the fractured formation is characterized by the slug flow. With the increase of the void fraction, the pressure wave velocity first decreases and then increases. For a void fraction between 0% and 16%, the pressure wave velocity is mainly of liquid slug, and decreases sharply. For a void fraction between 16% and 40%, the pressure wave velocity tends to be flat and constant. For a void fraction between 42% and 100%, the pressure wave velocity shows an increasing trend, and is mainly of bubble slug. With the decrease of the annulus well depth, the void fraction decreases and the pressure wave velocity falls. The pressure wave velocity increases with the back pressure of the kill circulating exhaust wellhead. For an annular void fraction between 0% and 13%, the gas slippage velocity has little influence on the pressure wave velocity. For an annular void fraction between 13% and 85%, the pressure wave velocity decreases with the gas slippage velocity. The time interval of the throttle valve follows the response time of the bottom hole pressure, and increases with the response time.

Key words: fractured gas reservoir; automatic kill; annulus polyphase; pressure wave velocity; gas slippage

引 言

川渝地区地质情况复杂, 面临异常高压、多压力系统、裂缝溶洞性地层, 井底易出现裂缝气、压差气等复杂气流, 以及循环排气后效时间长等施工难点, 需频繁循环排气和压井作业^[1-3]。目前, 国外的哈里伯顿公司已实现了实时自动压井系统, 并已投入使用; 国内的研究机构研发了多种压井模拟系统, 多采用低泵冲立压法控制井筒压力, 控压精度不高, 不能适应裂缝气地层窄密度窗口实时压井的需要。国内压井作业还没有实现自动化压井, 也无自动压井系统, 无法根据实时录井参数自动控制回压, 实时自动压井系统的难点是目标回压值与节流阀调节时间间隔确定^[4-6]。准确计算环空压力波传播速度, 可得到压力波沿环空的传播周期, 为节流阀开度调控间隔时间提供理论基础^[7-8]。

石油管道压力波速的研究始于 19 世纪, 随后, 国外学者推导了关于均质流、分层流的波速基本公式^[9-10]。到 21 世纪, 波速的研究更细致化, 压力波速应用至柴油、蒸汽、纳米铝热剂反应、交叉管道、气动管道、环道实验、输油管道、黏弹性管道、瞬态混相流、动力压力波、高低纬度变化等许多领域中进行研究, 并应用频率分析、小波变换及复系数方程等求解方法对波速求解^[11-12], 迄今为止, 压力波的研究仍在继续, 领域扩展至储气库采气、钻井控压钻井、大跨越管道油气输送、非常规(页岩气、煤层气等)油气储层改造中。

川渝地区裂缝性地层具有出气不规律、出气量大的特点, 井筒压力变化较为迅猛, 需要考虑自动化压井带来的自动监控、控制作用, 目前自动压井涉及压井方法的选择、复杂多相流的求解等难点, 自动压井技术尚不成熟, 仍需进一步研究。尽管前人对水平管道波速的研究很详尽^[13-15], 但目前尚没有针对自动压井相关环空压力波速的研究。由于压力波速影响井底压力的响应时间, 压力波沿环空传播的相长是调节节流阀时间间隔的重要判断依据, 本文分析了自动压井过程中回压产生的压力波沿环空传播变化特性, 可使压井工程师更直观地了解压力波传播速度以及传播影响的敏感因素, 为川渝裂缝性地层实时压井提供帮助。

1 环空压力波速模型建立

1.1 环空控制体多相流模型建立

在环空中求解环空的压力波速, 首先要求解环空气相空隙率、环空压力、环空中气液两相密度等基础参数, 作为压力波速求解的初始条件。因此, 首先建立环空控制体多相流模型。

环空中取一控制体, 气液连续数学模型^[4]如下所示:

$$\frac{\partial \left(A \sum_k \rho_k \phi_k \right)}{\partial t} + \frac{\partial \left(A \sum_k \rho_k \phi_k v_k \right)}{\partial s} = 0, \quad (1)$$

式中, A 为环空截面积; ρ_k 为气或钻井液相密度; ϕ_k 为气/钻井液相的体积分数; v_k 为气或钻井液相速度; k 为气/钻井液相; t 为时间; s 为环空长度。

环空控制体气液动量数学模型如下所示:

$$\frac{\partial \left(A \sum_k \rho_k \phi_k v_k \right)}{\partial t} + \frac{\partial \left(A \sum_k \rho_k \phi_k v_k^2 \right)}{\partial s} + A g \sum_k \rho_k \phi_k + \frac{\partial (A p)}{\partial s} + A p_f = 0, \quad (2)$$

式中, p_f 为摩阻梯度; g 为重力加速度.

裂缝性地层的溢流量数学模型如下所示:

$$Q = \frac{2.64 \times 10^{-20} K h (p_p^2 - p_b^2)}{(0.8 + \ln \xi) (T_e - 255) z \mu_g}, \quad (3)$$

其中

$$\xi = \max \left\{ 10, \frac{1.47 \times 10^{-9} t \left(\frac{K}{c \phi_g \mu_g} \right)}{r_w^2} \right\};$$

K 为裂缝性地层渗透率, md; h 为裂缝性地层裸露厚度, m; p_p 为原始地层流体压力, MPa; p_b 为井底压力, MPa; r_w 为裂缝性地层压力波及半径, m; T_e 为温度, °C; z 为压缩因子; μ_g 为气体黏度, Pa·s; c 为综合压缩系数, 无量纲.

将环空离散为 N 个网格, 沿井底向井口逐个网格求解, 对式(1)中气相连续方程半显式差分, 其格式如下:

$$\frac{[A \rho_g v_{sg}]_{i+1}^{n+1} - [A \rho_g v_{sg}]_i^{n+1}}{\Delta s} = \frac{[A \rho_g \phi_g]_i^n - [A \rho_g \phi_g]_{i+1}^n}{2\Delta t} - \frac{[A \rho_g \phi_g]_i^{n+1} - [A \rho_g \phi_g]_{i+1}^{n+1}}{2\Delta t}. \quad (4)$$

对式(1)中钻井液相连续方程半显式差分, 其格式如下:

$$\frac{(A v_{sl})_{i+1}^{n+1} - (A v_{sl})_i^{n+1}}{\Delta s} = \frac{(A \phi_1)_i^n + (A \phi_1)_{i+1}^n - (A \phi_1)_i^{n+1} - (A \phi_1)_{i+1}^{n+1}}{2\Delta t}. \quad (5)$$

对式(2)中钻井液相及气相动量方程半显式差分, 其格式如下:

$$(A p)_{i+1}^{n+1} - (A p)_i^{n+1} = K_1 + K_2 + K_3 + K_4, \quad (6)$$

$$K_1 = \frac{\Delta s}{2\Delta t} [(A(\rho_1 v_{sl} + \rho_g v_{sg}))_i^n + (A(\rho_1 v_{sl} + \rho_g v_{sg}))_{i+1}^n - (A(\rho_1 v_{sl} + \rho_g v_{sg}))_i^{n+1} - (A(\rho_1 v_{sl} + \rho_g v_{sg}))_{i+1}^{n+1}],$$

$$K_2 = \left[A \left(\frac{\rho_1 v_{sl}^2}{\phi_1} + \frac{\rho_g v_{sg}^2}{\phi_g} \right) \right]_i^{n+1} - \left[A \left(\frac{\rho_1 v_{sl}^2}{\phi_1} + \frac{\rho_g v_{sg}^2}{\phi_g} \right) \right]_{i+1}^{n+1}, \quad K_3 = -\frac{g \Delta s}{2} [(A \rho_1)_{i+1}^{n+1} + (A \rho_1)_i^{n+1}],$$

$$K_4 = -\frac{\Delta s}{2} \left[\left(A \left(\frac{\partial p}{\partial s} \right) \right)_{f_{ri}}^{n+1} + \left(A \left(\frac{\partial p}{\partial s} \right) \right)_{f_{ri+1}}^{n+1} \right],$$

式中, v_{sl} , v_{sg} 分别为钻井液相及地层气相的表观速度, m/s; ϕ_1 为持液率; ϕ_g 为空隙率; Δs 为控制体长度, m; Δt 为微元时间, s; ρ_1 为混相密度, kg/m³; p 为压力, MPa.

1.2 压力波速双流体数学模型建立

建立环空气相质量守恒方程:

$$\frac{\partial}{\partial t} (\phi \rho_g) + \frac{\partial}{\partial x} (\phi \rho_g u_g) = 0, \quad (7)$$

式中, ϕ 表示气相空隙率; ρ_g 表示气相密度, kg/m³; u_g 表示气相速度, m/s.

建立环空液相质量守恒方程:

$$\frac{\partial}{\partial t} [(1 - \phi) \rho_1] + \frac{\partial}{\partial x} [(1 - \phi) \rho_1 u_1] = 0, \quad (8)$$

式中, ρ_1 表示液相密度, kg/m³; u_1 表示液相速度, m/s.

建立气相动量守恒方程:

$$\frac{\partial}{\partial t} (\phi \rho_g u_g) + \frac{\partial}{\partial x} (\phi \rho_g u_g^2) + \frac{\partial}{\partial x} (\phi \rho_g) - \frac{\partial}{\partial x} [\phi (\tau_g^{fr} + \tau_g^{Re})] - M_{gi} + 4 \frac{\tau_g}{D} = 0, \quad (9)$$

式中, τ_g^{Re} 表示气相 Reynolds 应力, N/m²; τ_g^{fr} 表示气相剪切应力, N/m²; τ_g 表示气相管壁剪切应力, N/m².

建立环空液相动量守恒方程:

$$\frac{\partial}{\partial t} [(1-\phi)\rho_l u_l] + \frac{\partial}{\partial x} [(1-\phi)\rho_l u_l^2] + \frac{\partial}{\partial x} [(1-\phi)\rho_l] - \frac{\partial}{\partial x} [(1-\phi)(\tau_1^{fr} + \tau_1^{Re})] - M_{li} + \frac{4\tau_1}{D} = 0, \quad (10)$$

式中, τ_1 表示液相管壁剪切应力, N/m^2 ; τ_1^{Re} 表示液相 Reynolds 应力, N/m^2 ; τ_1^{fr} 表示液相剪切应力, N/m^2 .

气相与液相的动量交换^[6]表示为

$$M_{gi} = -M_{li}^{nd} - M_{li}^d + (\tau_{li}^{fr} + \tau_{li}^{Re}) \frac{\partial \phi_1}{\partial x} + \frac{\partial(\phi \sigma_s)}{\partial x} + \frac{\partial(\phi p_g)}{\partial x} - \frac{\partial(p_l)}{\partial x}, \quad (11)$$

式中, M_{li}^{nd} 表示液相非拖拽力动量交换, N/m^3 ; M_{li}^d 表示液相拖拽力的动量交换, N/m^3 ; τ_{li}^{fr} 表示液相界面剪切力, N/m^2 ; τ_{li}^{Re} 表示液相界面 Reynolds 应力, N/m^2 ; σ_s 表示表面张力, N/m^2 ; p_g 表示气相压力, MPa.

非拖拽力引发的气液相界面产生的动量交换公式^[6]表示为

$$M_{li} = M_{li}^{nd} + M_{li}^d + p_{li} \frac{\partial(\phi_1)}{\partial x} - (\tau_{li}^{fr} + \tau_{li}^{Re}) \frac{\partial \phi_1}{\partial x}, \quad (12)$$

式中, p_l 表示液相压力, MPa; ϕ_1 表示持液率, %.

钻井液流动过程中, 气相与液相的动量交换量公式为

$$M_{li}^{nd} = C_{vm} \phi \rho_l a_{vm} - 0.1 \phi \rho_l u_r \frac{\partial u_r}{\partial x} - 0.1 \rho_l u_r^2 \frac{\partial \phi}{\partial x}, \quad (13)$$

式中, C_{vm} 表示虚拟质量力系数; a_{vm} 表示虚拟质量加速度, m/s^2 ; u_r 表示滑脱速度, m/s .

拖拽力产生的动量交换量公式为

$$M_{li}^d = \frac{3}{8} \frac{C_D}{r} \rho_l \phi u_r^2, \quad (14)$$

式中, C_D 表示相间阻力系数, 无量纲.

气液的含量之和表示为

$$\phi + \phi_1 = 1. \quad (15)$$

由于裂缝气地层出气不规律, 环空采用段塞流的虚拟质量力系数参数^[7], 表示为

$$C_{vm} = 3.3 + 1.7 \frac{3L_q - 3R_q}{3L_q - R_q}, \quad (16)$$

式中, L_q 表示气泡长度, m ; R_q 表示气泡宽度, m .

气相滑脱速度表示为

$$u_r = u_g - u_l. \quad (17)$$

裂缝气段塞流的相间阻力系数为^[7]

$$C_D = 110(1-\phi)^3 R_q. \quad (18)$$

环空钻井液的压力为

$$p_l = p - 0.25 \rho_l \phi u_r^2. \quad (19)$$

液相压力波速与气相压力波速关系为

$$dp_l/d\rho_l = c_l^2, \quad dp_g/d\rho_g = c_g^2, \quad (20)$$

式中, c_l 表示液相波速, m/s ; c_g 表示气相波速, m/s .

通过对双流体质量守恒及动量守恒整理得到

$$F_i(\mathbf{X} + \delta \mathbf{X}) = F_i(\mathbf{X}) + \sum_{j=1}^N \frac{\partial F_i}{\partial x_j} \delta x_j + o(\delta \mathbf{X}^2). \quad (21)$$

做如下假设:

$$J = \sum_{j=1}^N \partial F_i / x_j, \quad (22)$$

经过小扰动变换, 可得到

$$F(\mathbf{X} + \delta\mathbf{X}) = F(\mathbf{X}) + \mathbf{J} \cdot \delta\mathbf{X} + o(\delta\mathbf{X}^2). \quad (23)$$

变量 $\mathbf{X}(\phi, p, u_g, u_l)^T$ 为

$$\mathbf{X} = \mathbf{X}_0 + \delta\mathbf{X} \cdot \exp[i(\omega t - Kx)]. \quad (24)$$

双流体模型的压力波速模型可整理为如下行列式:

$$\begin{vmatrix} M_1 & M_2 & M_3 & M_4 \\ -\rho_1 w & \phi_1 w / c_1^2 & 0 & -K \phi_1 \rho_1 \\ M_5 & M_6 & M_7 & M_8 \\ M_9 & M_{10} & M_8 & M_{11} \end{vmatrix} = 0, \quad (25)$$

其中

$$\begin{aligned} M_1 &= \left(\rho_g + c_p \phi \rho_l \frac{u_r^2}{c_g^2} \right) w, \quad M_2 = \frac{\phi}{c_g^2} [1 - c_p(1 - \phi)] \frac{u_r^2}{c_1^2} w, \\ M_3 &= - \left[\phi \rho_g K + 2c_p \phi(1 - \phi) \rho_l \frac{u_r}{c_1^2} w \right], \quad M_4 = 22c_p \phi(1 - \phi) \rho_l \frac{u_r}{c_1^2} w, \\ M_5 &= \rho_l u_r^2 K (-\phi c_p + c_r - c_{m1} + c_{m2}), \quad M_6 = -\phi K \left[1 - (1 - \phi) \frac{c_p u_r^2}{c_1^2} + c_i \frac{u_r^2}{c_1^2} \right], \\ M_7 &= \phi (\rho_g + c_{vm} \rho_l) w - i \left(\frac{3}{4} \frac{C_D}{r} \rho_l \phi u_r + \frac{4}{D} f_g \rho_g u_g \right), \quad M_8 = -c_{vm} \phi \rho_l w + i \frac{3}{4} \frac{C_D}{r} \rho_l \phi u_r, \\ M_9 &= \rho_l u_r^2 K ((1 - \phi) c_p - 2c_r - c_{m2}), \quad M_{10} = -K \left(1 - \phi + c_r \phi \frac{u_r^2}{c_1^2} \right), \\ M_{11} &= \rho_l [(1 - \phi) + \phi c_{vm}] w - i \left(\frac{3}{4} \frac{C_D}{r} \rho_l \phi u_r + \frac{4}{D} f_l \rho_l u_l \right), \end{aligned}$$

c_{m1}, c_{m2}, c_{m2} 分别为 0.1, 0.1, 0.25.

双流体压力波速模型如下:

$$c = \frac{\left| \frac{w}{R^+(K)} - \frac{w}{R^-(K)} \right|}{2}, \quad (26)$$

式中, K 表示波数; w 表示扰动频率, Hz.

液相摩阻系数 f_l 可以表示为

$$f_l = 0.013 + 0.23 \times 10^{-5} Re_1, \quad (27)$$

式中, Re_1 表示液相 Reynolds 数.

2 模型求解流程

2.1 环空压力多相压力波速求解思路

将环空离散成 n 个网格单元, 对每个离散单元 i 分别利用半显式差分的方法求解多相流模型, 获得环空多相流空隙率、气液密度、气体滑脱速度等参数; 将每个单元 i 的多相流基础参数代入双流体数学公式(25), 得到离散单元 i 的压力波速(具体求解技术路线如图 1 所示). 求解步骤如下:

- 第 1 步 获取环空多相流中压力、空隙率、气相密度、液相密度、气体滑脱速度等参数;
- 第 2 步 装双流体压力波速模型计算模块;
- 第 3 步 按照网格顺序, 获取压力波速.

2.2 压力波速模型验证

考虑虚拟质量力、环空沿程压力、相间阻力、气体滑脱、环空空隙率等因素, 计算机编程求解了环空双流模型, 分别对比了压力为 30 MPa^[15] 及含气率在 1% 及 20% 条件下^[16] 前人实验实测的压力波速(图 2), 通过对比, 编程求解的压力波速与前人实验测试数据具有一致性.

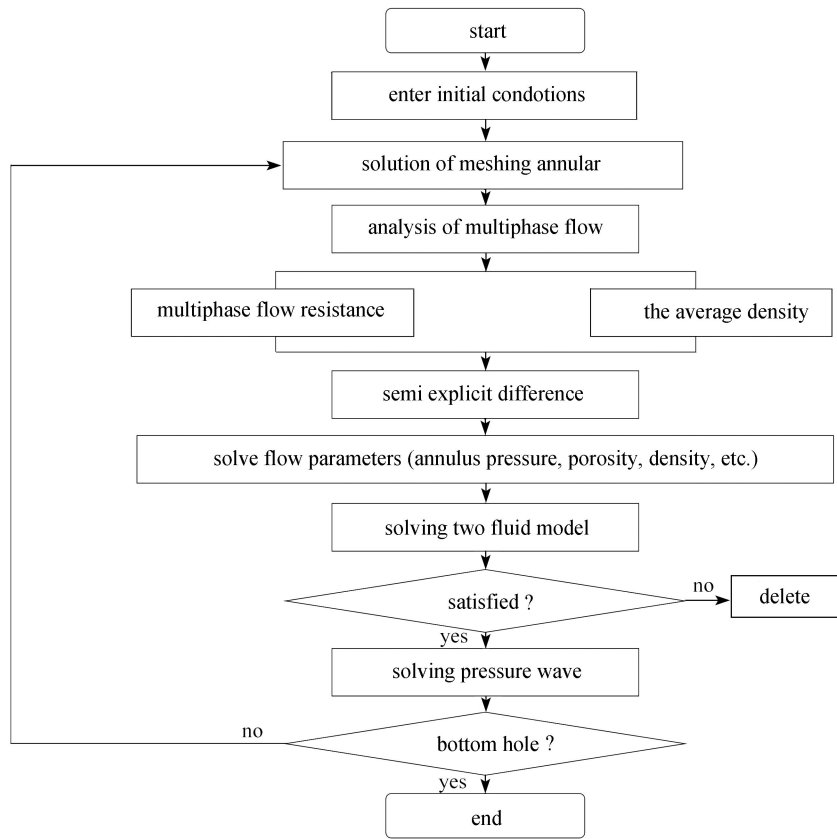


图 1 环空多相压力波速求解技术路线图

Fig. 1 The flowchart for solving the multiphase pressure wave velocity in annulus

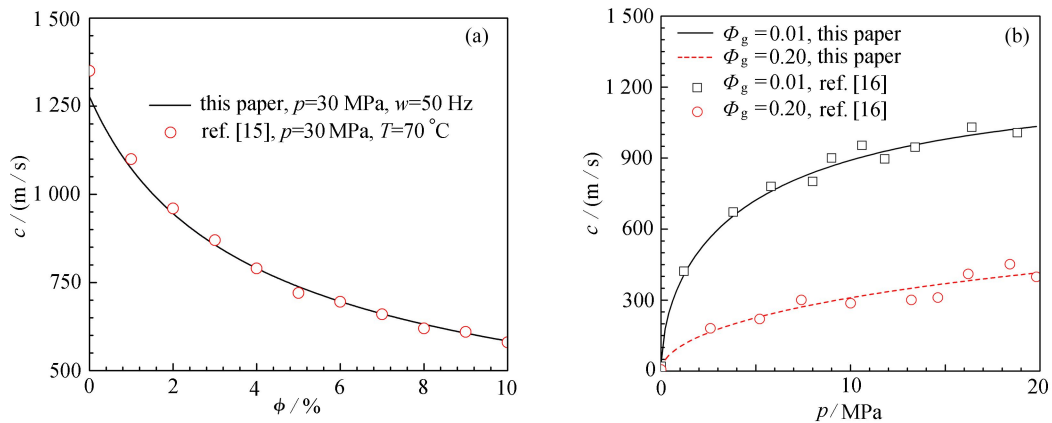


图 2 文献 [15-16] 的实验测试结果与本文模型计算压力波速对比: (a) 30 MPa 压力条件下压力波速对比结果; (b) 含气率在 1% 及 20% 条件下波速对比结果

Fig. 2 Comparisons between the experimental results of ref. [15-16] and the wave velocities calculated in this paper: (a) comparison of the wave velocity at a pressure of 30 MPa; (b) comparison of the wave velocity at gas contents of 1% and 20%

3 环空压力波速变化规律分析

PZ-5-3D 井位于四川省成都市彭州市葛仙山镇, 完钻层位: 雷四段 TL43-3 层, 靶点储层顶垂深 5787 m、储层底垂深 5827 m(如图 3 所示), 地质条件复杂, 上下地层压力系数差别大, 须家河组-小塘子组高压裂缝性气层发育(典型裂缝性地层), 分布广, 显示活跃且能量大, 小塘子组气层活跃, 钻至 5600 m 发生溢流, 钻井液黏度为 0.056 Pa·s, 钻井液密度为 1.66 g/cm³, 套管管柱弹性模量为 2.07 × 10¹¹, 地面大气压为 0.1 MPa, 段塞流气泡平均宽度为 0.002 m, 裂缝地层出气量为 0.33 L/s, BPT 节流循环排气回压, SPT 为立管压力。

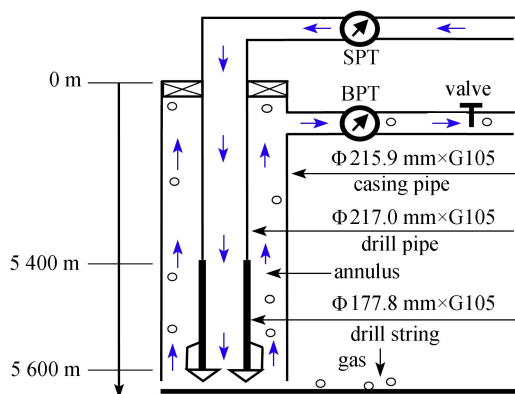


图3 自动压井气侵循环排气示意图

Fig. 3 Schematic diagram of automatic well killing gas invasion circulating exhaust

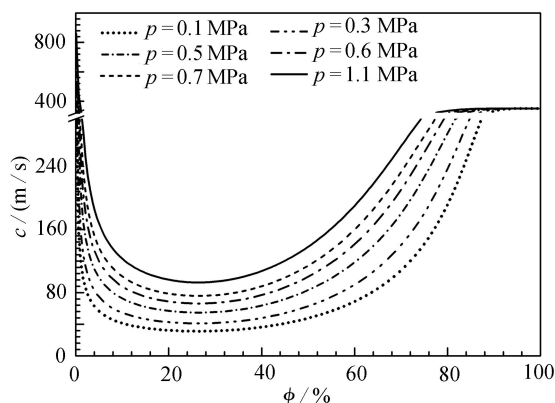


图4 裂缝气段塞流空隙率对压力波速的影响

Fig. 4 Effects of the crack gas slug flow void fraction on the pressure wave velocity

3.1 裂缝气段塞流空隙率对压力波速影响

图4为裂缝性地层出气,环空段塞流空隙率对压力波速的影响.随着压井环空压力波速增大,井底压力响应时间减小,节流阀调节时间间隔减小.流体弹性特点决定了流体的压缩性、气液能量耗散程度,从而影响压力波传递速度.随空隙率增大,压力波速呈现先减小后增大的趋势;裂缝气出气具有环空呈现段塞流型特点,环空空隙率在0%至16%区间同16%至82%区间比较,压力波速变化幅度大,环空空隙率在0%至16%区间,流体主要以液相弹性为主,压力波速呈现急剧下降趋势;空隙率在16%至45%区间,流体主要以气相弹性-液相弹性为主,压力波速趋于恒定值;环空空隙率在45%至70%区间,流体主要以气相弹性为主,压力波速呈现增大趋势;环空空隙率大于70%区间压力波速区域稳定.

3.2 裂缝性气侵速度对压力波速影响

图5为裂缝性地层气侵流量 $v=0.01\text{ L/s}, 0.08\text{ L/s}, 0.15\text{ L/s}, 0.22\text{ L/s}, 0.29\text{ L/s}, 0.33\text{ L/s}$ 条件下,压力波速沿环空变化特性分析.随环空空隙率减小,压力波速整体呈现减小趋势;当井底气侵流量增大时,环空整体空隙率也呈现增大趋势,压力波速呈现降低趋势,各井段压力响应时间延长,压井节流阀调节间隔增大.当气侵量较小时,在小于等于721 m井深时,压力波速急剧增大,从132 m/s增大至958 m/s;当气侵流量较大时,环空遭受气侵程度较大,压力波速沿着整个环控段呈现线性增大趋势,井底压力响应呈现减小趋势,节流阀调阀时间间隔呈现减小趋势.

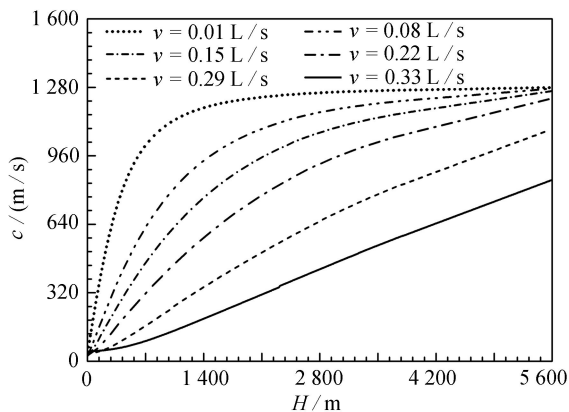


图5 裂缝性地层气侵流量对压力波速的影响

Fig. 5 Effects of the gas invasion velocity on the pressure wave velocity in the fractured gas reservoir

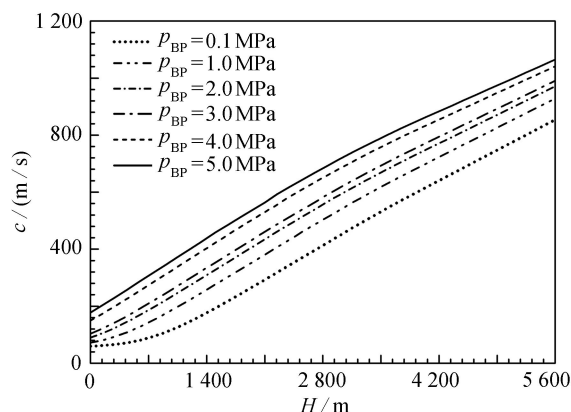


图6 压井节流阀回压对压力波速的影响

Fig. 6 Effects of the throttle valve back pressure on the pressure wave velocity

表1为气体滑脱速度对压力波速影响数据表.在少量含气率的条件下,由于流体介质主要以液相为主,虽然气体滑脱速度增大,但对气液两相平均体积、平均密度影响不大,此阶段气体滑脱对压力波速的影响不大.当气体含量大于13%时,气体滑脱速度开始对压力波速产生影响,这是由于气体沿着环空向井口运移过程中,气体滑脱速度的增大,使得气体膨胀体积更大,此阶段气体体积对气液平均密度、环空压力影响逐渐增大,因此,此阶段气体滑脱对压力波速的影响逐渐增大.当含气率为98.1%时,滑脱速度0.8 m/s同0.08 m/s比较,压力波速从87.31 m/s增大至349.99 m/s,压力波速增大了262.68 m/s,同87.31 m/s比较,增大了200.86%.

4 结 论

本文以川渝地区裂缝性地层气侵自动压井为背景,结合压井节流阀动作产生的压力波动源,分析了沿环空多相流动方向的压力波速变化特性,主要得到以下结论:

1) 由于裂缝气地层出气比较迅猛,环空多相流流型主要考虑段塞流流型;环空空隙率在0%至16%区间,压力波速呈现急剧减小趋势;环空空隙率在16%至45%区间,压力波速呈现增大趋势;环空空隙率在45%至70%区间,压力波速呈现增大趋势;环空空隙率大于70%区间,压力波速趋于稳定.

2) 与常规油气输送管道比较,压井循环排气过程中,压力波速计算不仅要考虑环空中时刻变化的空隙率、节流阀动作产生的回压值、气体滑脱速度、环空深度等因素,也要考虑虚拟质量力的因素,在压井环空中,考虑虚拟质量力与不考虑虚拟质量力相比,压力波速增大了6.25倍.

3) 在压井循环排气操作中,节流阀频繁动作产生回压,达到控制环空循环排气的目的,从而平衡井底压力;节流阀动作间隔需要考虑压力波动的传播周期,压井工程师应尽量控制节流阀动作产生的稳态回压周期大于压力波沿环空传播一个周期时间,随压井环空压力波速增大,井底压力响应时间减小,节流阀调节时间间隔减小.

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